

Catalysis Today 45 (1998) 23-28



# Partial oxidation of light alkanes by $NO_x$ in the gas phase

K. Otsuka\*, R. Takahashi, K. Amakawa, I. Yamanaka

Department of Chemical Engineering, Tokyo Institute of Technology, Ookayama, Meguro-ku, Tokyo 152, Japan

### Abstract

Partial oxidations of  $CH_4$ ,  $C_2H_6$ ,  $C_3H_8$ , and iso- $C_4H_{10}$  with  $O_2$  were promoted by addition of NO in the gas phase. The addition of NO increased the conversion rate of alkanes and decreased the initiation temperatures for the reactions. Moreover, selectivities and yields to oxygenates, aldehydes, ketones and alcohols, were remarkably improved by the addition of NO. The maxima of one-pass yields of oxygenates were 7% for  $CH_4$ , 11% for  $C_2H_6$ , 13% for  $C_3H_8$ , and 29% for iso- $C_4H_{10}$ . It is suggested that  $NO_2$  produced from NO and  $O_2$  is the initiator for the oxidation of light alkanes. Alkyl nitrite was proposed as the reaction intermediate for the formation of oxygenates. The alkyl nitrite decomposes into oxygenates and NO that works as catalyst for the activation of  $O_2$  and the oxidation of alkanes. © 1998 Elsevier Science B.V. All rights reserved.

Keywords: Partial oxidation; CH<sub>4</sub>; C<sub>2</sub>H<sub>6</sub>; C<sub>3</sub>H<sub>8</sub>; NO<sub>x</sub>

### 1. Introduction

De-NO<sub>x</sub> is one of the most important subjects for sustaining the lives of creature on the earth because NO<sub>x</sub> are poisons due to their high reactivities against organic compounds. However, we believe that this high reactivity of NO<sub>x</sub> could be applied for activation and oxidation of alkanes, synthesizing useful oxygenates.

Chemical utilization of natural gas (CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, and C<sub>3</sub>H<sub>8</sub>) as a feed stock is an attractive subject for chemical industry. However, it is difficult to convert light alkanes directly into useful oxygenates, such as aldehydes, ketones, and alcohols, due to their low reactivities. Many chemists have studied a great number of catalytic oxidation systems [1–3] and non-catalytic radical chain reactions in the gas phase [4] to convert light alkanes, especially CH<sub>4</sub>, to oxygenates. However, one-pass yields for the sum of HCHO

The aims of this work are to demonstrated the effect of NO on the formation of oxygenates especially from  $C_2H_6$ ,  $C_3H_8$ , and iso- $C_4H_{10}$  and to get informations about the reaction mechanism of the formation of the oxygenates.

## 2. Experimental

The oxidations of light alkanes,  $CH_4$ ,  $C_2H_6$ ,  $C_3H_8$  and iso- $C_4H_{10}$ , were carried out by using a conven-

and MeOH were lower than 5% for most of the works reported so far for the oxidation of CH<sub>4</sub>. Irusta [5] and Haruta [6] recently reported the effect of NO (HNO<sub>3</sub>) on the oxygenation of CH<sub>4</sub> to HCHO (<4% yield) in the gas phase at  $560^{\circ}$ C. Since long time ago, it has been known that the oxidation of CH<sub>4</sub> with O<sub>2</sub> can be accelerated by addition of NO [7]. However, detailed reaction mechanism for the formation of HCHO has not been cleared yet. Moreover, there are a few studies focusing on the formation of oxygenates from C<sub>2</sub>H<sub>6</sub> and C<sub>3</sub>H<sub>8</sub> catalyzed by NO in the gas phase.

<sup>\*</sup>Corresponding author. Tel.: +81-3-5734-2143; fax: +81-3-5734-2879; e-mail: kotsuka@o.cc.titech.ac.jp

tional gas flow system. Standard experimental procedure was as follows. A gas mixture of light alkanes (20 kPa), O<sub>2</sub> (10 kPa), NO (2 kPa), balanced with He (total pressure 101 kPa, total flow rate =120 ml min<sup>-1</sup>) was introduced to a quartz tube reactor (i.d. 8 mm) at 450–650°C. Products were analyzed by an on-line gas chromatograph (Shimazu GC8A TCD with Porapak-Q, Porapak-T, and Molecular Sieve 5A columns). Conversions of alkanes, selectivities to products and product yields were calculated on the basis of the carbon numbers of the reactant alkanes.

### 3. Results and discussion

Fig. 1 shows the effects of addition of NO on the conversion rates of  $CH_4$ ,  $C_2H_6$ , and  $C_3H_8$ . In the absence of NO, the oxidations of  $C_3H_8$  and  $C_2H_6$  required the temperature above 500°C and that of  $CH_4$  did not occur at <650°C under this experimental conditions.

When NO was added to a mixture of alkane and  $O_2$ , the oxidations of  $C_3H_8$  and  $C_2H_6$  proceeded at  $400^{\circ}C$ , i.e.,  $100^{\circ}C$  lower temperature than those in the absence of NO. Moreover, oxidation of  $CH_4$  initiated at >450°C by addition of NO. When a mixture of  $C_3H_8$ ,  $C_2H_6$ , or  $CH_4$  with NO was introduced to the reactor without  $O_2$ , no conversion of these alkanes took place at  $600^{\circ}C$ . These results indicate that NO promotes the oxidations of light alkanes only in the

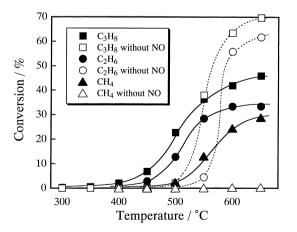


Fig. 1. Effect of the addition of NO on the conversion for the oxidations of light alkanes.

Table 1 Activation energy for the conversion rates of light alkanes with  $O_2$  in the gas phase

	Activation energy (kJ mol <sup>-1</sup> )				
	$C_3H_8$	C <sub>2</sub> H <sub>6</sub>	CH <sub>4</sub>		
Without NO	275	361	_		
With NO	107	138	208		

presence of  $O_2$ . The turnover numbers for the conversions of alkanes based on the NO introduced were 2.3 for  $C_3H_8$  (500°C), 2.8 for  $C_2H_6$  (550°C), and 2.9 for  $CH_4$  (650°C). These results suggest that NO works as a catalyst for the oxidation of the light alkanes.

Apparent activation energies for the conversion of CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, and C<sub>3</sub>H<sub>8</sub> with O<sub>2</sub> or with NO and O<sub>2</sub> are summarized in Table 1. The values were calculated from the slopes of the  $\ln r$  (r=conversion rate) vs. 1/Tplots. The activation energies for the conversion of C<sub>2</sub>H<sub>6</sub> and C<sub>3</sub>H<sub>8</sub> dramatically decreased by the addition of NO, as can be seen in Table 1. The activation energy for the oxidation of CH4 with O2 was not obtained because the oxidation of CH<sub>4</sub> did not proceed as described above. The activation energy for the oxidation of CH<sub>4</sub> with NO and O<sub>2</sub> was lower than those for the oxidations of  $C_2H_6$  and  $C_3H_8$  with  $O_2$ . These results suggest that the mechanisms for activation of the light alkanes with NO and O2 are very different from the non-catalytic radical-chain oxidations of alkanes with  $O_2$ .

The selectivities of products for the oxidation of the light alkanes with NO and O2 were also very different from those without NO. Fig. 2 shows the effects of temperature on the distribution of the products for the oxidation of  $C_3H_8$  with  $O_2$ . Alkenes ( $C_3H_6$  and  $C_2H_4$ ) were the major products and the selectivities to oxygenates (MeCHO, HCHO, MeOH, EtOH, EtCHO, and Me<sub>2</sub>CO) were less than 9% at the temperatures examined. While, in the presence of NO and  $O_2$ , much more oxygenates (MeCHO>HCHO>MeOH>EtOH, Me<sub>2</sub>CO, EtCHO) were formed for the oxidation of C<sub>3</sub>H<sub>8</sub> as indicated in Fig. 3. The selectivity to the sum of oxygenates is greater than 60% at <450°C. Nitroalkanes (MeNO<sub>2</sub>, EtNO<sub>2</sub>, 1-PrNO<sub>2</sub>, and 2-PrNO<sub>2</sub>), alkenes (C<sub>2</sub>H<sub>4</sub>, C<sub>3</sub>H<sub>6</sub>) and CO were formed as minor products at lower temperatures (350–450°C). When the reaction temperature was raised above 450°C, the selectivities to oxygenates decreased and

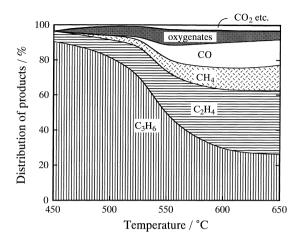


Fig. 2. Effects of temperature on the distribution of products for the oxidation of  $C_3H_8$  with  $O_2$ .

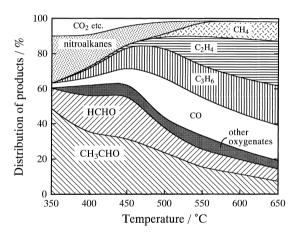


Fig. 3. Effects of temperature on the distribution of products for the oxidation of  $C_3H_8$  with (NO+O<sub>2</sub>).

nitroalkanes disappeared at >550°C. In contrast, the selectivities to alkenes ( $C_3H_6$ ,  $C_2H_4$ ),  $CH_4$  and CO increased considerably at >550°C. This large difference in the product distributions between Figs. 2 and 3 suggests that the reaction mechanism for oxidation of  $C_3H_8$  with (NO+O<sub>2</sub>) is quite different from the noncatalytic auto-oxidation mechanism.

Fig. 4 shows the effects of temperatures on the yield of the sum of oxygenates for the oxidations of  $CH_4$ ,  $C_2H_6$ , and  $C_3H_8$  with  $(NO+O_2)$  and with  $O_2$ . The product distributions in oxygenates were roughly as  $HCHO\gg MeOH> MeCHO$  for oxidation of  $C_2H_6$ , and

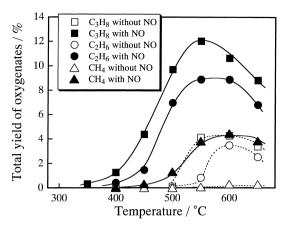


Fig. 4. Effect of the addition of NO on the yields of oxygenates for the oxidations of  $CH_4$ ,  $C_2H_6$ , and  $C_3H_8$  with  $O_2$ .

as HCHO $\gg$ MeOH for oxidation of CH<sub>4</sub>. The yields of the sum of oxygenates for the oxidations of CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub> and C<sub>3</sub>H<sub>8</sub> with (NO+O<sub>2</sub>) were remarkably higher than those with O<sub>2</sub> at all temperatures. Especially, dramatic enhancements in the selectivity to oxygenates were observed by the addition of NO at low temperature region, 350–500°C.

Fig. 5 shows the effects of partial pressure of NO on the formation rates of products for oxidation of  $C_3H_8$  with (NO+O<sub>2</sub>) at 420°C (low temperature region). The formation rates of each product increased with increasing P(NO).

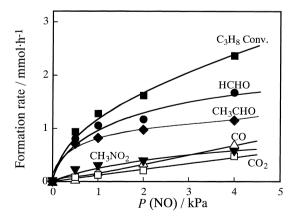


Fig. 5. Effect of P(NO) on the formation rates of products for the oxidation of  $C_3H_8$  with  $O_2$  at  $420^{\circ}C$ .  $P(C_3H_8)$  20 kPa,  $P(O_2)$  10 kPa, flow rate 120 ml min<sup>-1</sup>.

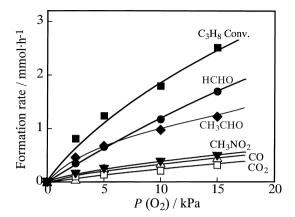


Fig. 6. Effect of  $P(O_2)$  on the formation rates of products for the oxidation of  $C_3H_8$  at 420°C.  $P(C_3H_8)$  20 kPa, P(NO) 2 kPa, flow rate 120 ml min<sup>-1</sup>.

Fig. 6 shows the effects of  $P(O_2)$  on the formation rates of each product at  $420^{\circ}$ C. The formation rates of each products increased with a rise in  $P(O_2)$ .

Fig. 7 shows the effects of P(NO) on the conversion of  $C_3H_8$  and on the yields of products at  $550^{\circ}C$ . It should be recalled that the oxidation of  $C_3H_8$  in high temperature region (> $500^{\circ}C$ ) proceeded in the absence of NO (Fig. 1). The conversion of  $C_3H_8$  in Fig. 7 did not change appreciably with increasing P(NO) mainly due to complete consumption of  $O_2$ . However, the selectivities to oxygenates increased and those to  $C_3H_6$  and  $C_2H_4$  decreased with increasing P(NO). These results suggest that reaction mechanism for the formation of products were changed dramatically by addition of NO also at high temperature region.

Optimum reaction conditions for the formation of oxygenates were examined for the oxidations of  $CH_4$ ,  $C_2H_6$ ,  $C_3H_8$  and iso- $C_4H_{10}$ . The results are shown in

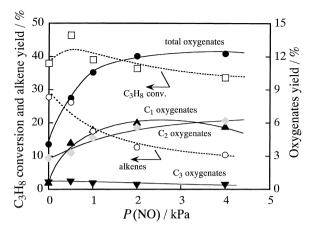


Fig. 7. Effect of P(NO) on the oxidation of  $C_3H_8$  at 550°C.  $P(C_3H_8)$  20 kPa,  $P(O_2)$  10 kPa, flow rate 120 ml min<sup>-1</sup>.

Table 2. Fairly good yields of the sum of oxygenates were obtained for each light alkane under the reaction conditions in Table 2. Under these conditions, only a trace of nitroalkanes and  $N_2$  was observed. Therefore, most of the NO introduced was remained in the gas mixture at the outlet. This observation indicates that NO can be recycled as catalyst for the oxidation of light alkanes.

As described above, co-addition of NO and O<sub>2</sub> remarkably accelerated the rate of conversion of light alkanes and the formation rates of oxygenates. The reaction between NO and alkanes did not take place in the absence of O<sub>2</sub>. These observations suggest that NO<sub>2</sub> would work as an initiator or an active oxidant in the oxidations. Thus, it is speculated that some NO<sub>2</sub>-containing hydrocarbons could be the reaction intermediate for the formation of oxygenates. In fact, small amounts of nitroalkanes (MeNO<sub>2</sub>, EtNO<sub>2</sub> and PrNO<sub>2</sub>)

Table 2 Yields of oxygenates under optimum conditions

Reactant	Temparature (°C)	Pressure (kPa)		rrature (°C) Pressure (kPa) Conversion		Conversion (%)	Yield (based on the alkanes reacted) (%)			
		Alkane	$O_2$	NO		НСНО	МеОН	МеСНО	Acetone	Total
CH <sub>4</sub> <sup>a</sup>	600	5.0	2.5	0.5	17	6.5	0.2	_	_	6.7
$C_2H_6^a$	600	5.0	2.5	0.5	31	9.5	0.8	1.0		11.3
$C_3H_8^{\ a}$	550	10	5.0	1.0	38	5.6	1.8	5.3	0.2	12.9
$iso-C_4H_{10}^{\ \ b}$	425	10	15	4.0	53	5.6	1.2	3.7	18.2	28.7

<sup>&</sup>lt;sup>a</sup>Flow rate=120 ml min<sup>-1</sup>.

<sup>&</sup>lt;sup>b</sup>Flow rate=60 min<sup>-1</sup>.

Table 3 Decomposition of *tert*-BuONO at 400°C

Conditions	Conversion (%)	Formation rate (µmol min <sup>-1</sup> )					
		Acetone	НСНО	СО	CO <sub>2</sub>	CH <sub>3</sub> NO <sub>2</sub>	
Не	82	26	trace	0	0.1	1.0	
$O_2$	100	29	8.0	51	6.4	4.8	
$O_2+NO$	100	27	8.8	59	3.2	6.0	

Reaction conditions: P(tert-BuONO)=1.1 kPa, P(O<sub>2</sub>) 10 kPa, P(NO) 1.0 kPa, flow rate 60 ml min<sup>-1</sup> (balanced with He).

were formed at low temperatures as shown in Fig. 3. Therefore, decomposition reactions of 1-PrNO $_2$  and 2-PrNO $_2$  were carried out to get information about the reaction mechanisms. The results showed that the major product was  $C_3H_6$  in both cases. This result suggests that nitroalkane could not be the precursor for the formation of oxygenates.

Table 3 shows the results of the decomposition of *tert*-BuONO. The decomposition of *tert*-BuONO in a stream of He at  $400^{\circ}$ C produced acetone as main products, but a deposition of carbon on the wall of reactor was observed. When  $O_2$  or a mixture of NO and  $O_2$  was added, the formation rate of acetone was not changed but the formation of HCHO, CO, CO<sub>2</sub> and CH<sub>3</sub>NO<sub>2</sub> were observed instead of the carbon deposition. These results strongly suggest that alkyl nitrite could be the reaction intermediate for the formation of oxygenates in the oxidation of light hydrocarbons with (NO and  $O_2$ ).

On the bases of the results in this work together with the mechanism suggested for the radical-chain auto-oxidation [8,9], we propose Scheme 1 for the oxidation of light alkanes catalysed by NO. NO<sub>2</sub> is an initiator for the formation of alkyl radicals (Eq. 2). The alkyl radicals (R•) reacts with NO<sub>2</sub> producing RONO as an reaction intermediate for the formation of oxygenates (Eq. 3). Then, RONO decomposes to RO• regenerating NO (Eq. 4). RO• decomposes to aldehydes or acetone (Eqs. 5, 5′, 5″) and CH<sub>3</sub>• which is further oxidized into HCHO, CO and CO<sub>2</sub> (Eq. 6). RNO<sub>2</sub> formed in Eq. 3′ may decompose into alkenes and CO.

On the other hand, it is reasonable to assume that for the oxidations of light alkanes with  $O_2$  in the absence of NO proceed through the radical-chain auto-oxidation mechanism in Scheme 2. Peroxy–alkyl radicals work as intermediates for the oxidation of light

$$NO + 1/2 O_2 \longrightarrow NO_2$$

$$RH + NO_2 \longrightarrow R \cdot + HNO_2$$

$$R \cdot + NO_2 \longrightarrow RONO$$

$$RONO \longrightarrow RO \cdot + NO$$

$$RONO \longrightarrow RO \cdot + NO$$

$$RO \cdot \longrightarrow HCHO + R' \cdot$$

$$(R = CH_3, C_2H_5, n-C_3H_7)$$

$$RO \cdot \longrightarrow CH_3CHO + CH_3 \cdot$$

$$(R = iso-C_3H_7)$$

$$RO \cdot \longrightarrow CH_3COCH_3 + CH_3 \cdot$$

$$(R = tert-C_nH_0)$$

$$(S'')$$

$$CH_3$$
·  $\xrightarrow{O_2, NO_2}$  HCHO,  $CO, CO_2$  (6)

Scheme 1.

alkanes (Eqs. 7 and 8). In this mechanism, alkenes are produced as the main products of the oxidation (Eqs. 9 and 10) as in fact observed in Fig. 2.

In the case of the catalytic oxidation of alkanes by NO at low temperature region, the oxidation proceed through Scheme 1. While, we cannot neglect the contribution of Scheme 2 for the oxidation with NO and  $O_2$  at high temperature region.

$$RH + O_2 \longrightarrow R \cdot + HO_2 \cdot \tag{7}$$

$$R \cdot + O_2 \longrightarrow RO_2 \cdot$$
 (8)

$$RO_2$$
  $\longrightarrow$  alkene +  $HO_2$  (9)

$$RO_2$$
·  $\longrightarrow$  R'CHO + HO· (9')

$$R \cdot \longrightarrow \text{alkene} + H \cdot$$
 (10)

Scheme 2.

## Acknowledgements

A part of this work has been carried out as a research project of the Japan Petroleum Institute commissioned by the Petroleum Energy Center with the subsidy of the Ministry of International Trade and Industry.

## References

- [1] R. Pitchai, K. Klier, Catal. Rev. -Sci. Eng. 28 (1986) 13.
- [2] M.F. Brown, N.D. Parkyns, Catal. Today 8 (1991) 305.

- [3] K. Otsuka, M. Hatano, in: E.E. Wolf (Ed.), Methane Conversion by Oxidative Process, Van Nostrand Reinhold, New York, 1992, p. 72.
- [4] G.A. Fould, B.F. Gray, Fuel Proc. Tech. 42 (1995) 129.
- [5] S. Irusta, E.A. Lombardo, E.E. Miró, Catal. Lett. 29 (1994) 339
- [6] L.B. Han, S. Tsubota, M. Haruta, Chem. Lett. (1995) 931.
- [7] T.E. Layng, R. Soukop, Ind. Eng. Chem. 20 (1928) 1052.
- [8] O.P. Strausz, J.W. Lown, H.E. Gunning, in: C.H. Bamford, C.F.H. Tipper (Eds.), Comprehensive Chemical Kinetics, vol. 5, Elsevier, Amsterdam, 1972.
- [9] R.T. Pollard, in: C.H. Bamford, C.F.H. Tipper (Eds.), Comprehensive Chemical Kinetics, vol. 17, Elsevier, Amsterdam, 1977.